

(51) International Patent Classification⁶ :

B01D 61/00, G01N 33/48

A1

(11) International Publication Number:

WO 96/04067

(43) International Publication Date:

15 February 1996 (15.02.96)

(21) International Application Number: PCT/GB95/01834

(22) International Filing Date: 2 August 1995 (02.08.95)

(30) Priority Data:

9415560.3	2 August 1994 (02.08.94)	GB
9421682.7	27 October 1994 (27.10.94)	GB
9422870.7	12 November 1994 (12.11.94)	GB
9422875.6	12 November 1994 (12.11.94)	GB

(71) Applicant (for all designated States except US): FSM TECHNOLOGIES LTD. [GB/GB]; 6 Dunrobin Court, North Avenue, Clydebank Business Park, Clydebank G81 2NT (GB).

(72) Inventor; and

(75) Inventor/Applicant (for US only): HOOD, Robert, Gordon [GB/GB]; 3 Station Rise, Lochwinnoch, Renfrewshire PA12 4NA (GB).

(74) Agent: MURGITROYD & CO.; 373 Scotland Street, Glasgow G5 8QA (GB).

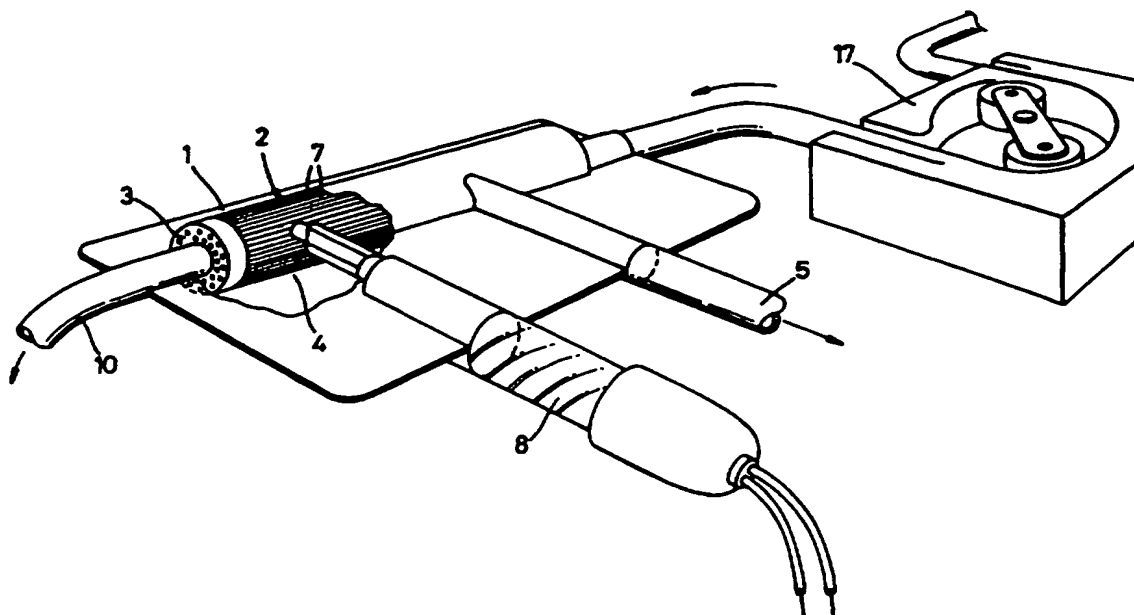
(81) Designated States: AM, AT, AU, BB, BG, BR, BY, CA, CH, CN, CZ, DE, DK, EE, ES, FI, GB, GE, HU, IS, JP, KE, KG, KP, KR, KZ, LK, LR, LT, LU, LV, MD, MG, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, TJ, TM, TT, UA, UG, US, UZ, VN, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG), ARIPO patent (KE, MW, SD, SZ, UG).

Published

With international search report.

Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.

(54) Title: MEMBRANE FILTER UNIT



(57) Abstract

The present invention describes a device to process a fluid, the device having a membrane filter, wherein an agent able to detect or cause modification of at least one component of said fluid is localised in said device, preferably on the membrane. The device is arranged to filter the fluid by cross-flow filtration. A preferred form of membrane filter is hollow fibre membrane(s), especially a single hollow fibre membrane. Space between the exterior of the membrane and the inside surface of the outer casing of the device may be completely or partially filled with a solid material, which may contain the agent.

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	GB	United Kingdom	MR	Mauritania
AU	Australia	GE	Georgia	MW	Malawi
BB	Barbados	GN	Guinea	NE	Niger
BE	Belgium	GR	Greece	NL	Netherlands
BF	Burkina Faso	HU	Hungary	NO	Norway
BG	Bulgaria	IE	Ireland	NZ	New Zealand
BJ	Benin	IT	Italy	PL	Poland
BR	Brazil	JP	Japan	PT	Portugal
BY	Belarus	KE	Kenya	RO	Romania
CA	Canada	KG	Kyrgyzstan	RU	Russian Federation
CF	Central African Republic	KP	Democratic People's Republic of Korea	SD	Sudan
CG	Congo	KR	Republic of Korea	SE	Sweden
CH	Switzerland	KZ	Kazakhstan	SI	Slovenia
CI	Côte d'Ivoire	LI	Liechtenstein	SK	Slovakia
CM	Cameroon	LK	Sri Lanka	SN	Senegal
CN	China	LU	Luxembourg	TD	Chad
CS	Czechoslovakia	LV	Latvia	TG	Togo
CZ	Czech Republic	MC	Monaco	TJ	Tajikistan
DE	Germany	MD	Republic of Moldova	TT	Trinidad and Tobago
DK	Denmark	MG	Madagascar	UA	Ukraine
ES	Spain	ML	Mali	US	United States of America
FI	Finland	MN	Mongolia	UZ	Uzbekistan
FR	France			VN	Viet Nam
GA	Gabon				

1 "Membrane Filter Unit"

2

3 This invention relates to the membrane units for
4 filtration or analysis or to support cell culture.

5

6 It is known to control chemical and biological
7 processes performed in process vessels by withdrawing
8 samples, filtering the samples to remove undissolved,
9 colloidal or suspended particles or materials of high
10 molecular weight and then subjecting the filtrate to
11 chemical tests. The filtrate may optionally be
12 returned to the mother liquor after analysis. The
13 whole operation may be time consuming and laborious and
14 the quantities of filtrate removed may affect the
15 course of the chemical or biological process.
16 Alternative analytical methods that are available for
17 "real-time" analysis within the process vessel are
18 often highly specific to the particular analyte,
19 provide only very restricted information and may be
20 expensive.

21

22 It would be advantageous to have a system that allowed
23 continuous sampling without causing substantial change
24 to the total volume of the process liquor, but which

1 automatically removed substances over a chosen particle
2 size or over a chosen molecular weight by filtration,
3 and returned the filtrate to the process liquor. It
4 would be especially advantageous if the system involved
5 the temporary removal of only a minimal amount of the
6 process liquor from the process vessel.

7
8 Additionally many process liquors contain soluble or
9 dispersed ingredients which require to be separated,
10 combined, monitored, analysed or controlled. These
11 ingredients may be reactants, intermediates or products
12 of the process. However, analysis and/or control are
13 frequently made difficult, or even impossible, by the
14 presence of substances in suspension or of substances
15 of lower or higher concentrations in solution. The
16 problems which arise because of the presence of these
17 substances include obstruction of the membrane pores,
18 discoloration or turbidity of the liquor making
19 colorimetric analysis difficult, and chemical
20 imbalances which make analysis and processing
21 difficult, and contamination, which can lead to the
22 rapid deterioration of, for example, cells and/or
23 sensor elements. Micro- and ultra-filtration membranes
24 exist which allow the separation of particles such as
25 proteins, cells, cell debris and bacteria, from one
26 another, but separation of these materials or
27 substances from one another can be difficult,
28 inconsistent and time consuming. The delay in the
29 response time may be unacceptable.

30
31 The above also applies where it is desired to grow
32 cells in culture on a membrane or other support and
33 where the cells or a sample thereof are to be exposed
34 to challenge substances.

35
36 The present invention provides a device to process a

1 fluid, the device having a membrane filter, wherein an
2 agent able to detect or cause modification of at least
3 one component of said fluid is localised in said
4 device, for example is located on or in proximity to
5 said filter.

6
7 The device of the invention is arranged so that
8 filtration of the fluid occurs by cross-filtration, ie
9 the fluid to be processed flows along the surface of
10 the membrane and is not directed perpendicularly
11 towards the membrane.

12
13 In a preferred embodiment the device of the invention
14 comprises an agent (sensor) able to detect a component
15 in the process liquor, which may be, for example,
16 located in the test fluid.

17
18 Optionally, the detected or modified component is
19 released back into the fluid.

20
21 The fluid to be processed may comprise a liquid
22 (optionally including dissolved or suspended solid
23 particles). Optionally the fluid to be processed
24 comprises a gas. Alternatively the fluid to be
25 processed is a liquid suspension of cells or parts of
26 cells.

27
28 In one embodiment, the device of the invention is for
29 use in a continual processing operation, that is to say
30 a constant supply of the liquid to be processed flows
31 through the device. In this embodiment it is preferred
32 that the agent is self-regenerating, although it may
33 also be possible in certain circumstances for the agent
34 to be artificially regenerated at intervals during the
35 processing operation or even for the agent, optionally
36 together with the filter on which the agent is located,

1 to be replaced periodically as required. It is
2 possible for the device to be adapted to support cell
3 growth on the membrane, the fluid flowing through the
4 membrane comprising all of the nutrients needed to
5 support cell growth. Such an arrangement provides a
6 useful experimental tool as well as a means of
7 culturing and challenging cells to provide an in vitro
8 diagnosis, for example by subsequent exposure of the
9 cells to antibodies or other challenge substances.

10

11 In an alternative embodiment, the device of the
12 invention is arranged for single use applications, such
13 as testing body fluids eg blood, plasma, urine,
14 synovial fluid and the like. Generally the device will
15 be wholly disposable or will be partially disposable
16 for such applications.

17

18 Optionally, the membrane may be selected to filter out
19 a particular molecular size range so that only
20 molecules below a certain size are present in the
21 filtrate. The agent may be located on the post-
22 filtration side of the filter where the agent to be
23 modified is present in the filtrate. Alternatively the
24 agent may be located on the pre-filtration side of the
25 filter.

26

27 The agent may be located on the filter membrane by any
28 convenient means, for example hydrophobic or
29 hydrophilic attraction with the membrane surface or
30 chemical bonding, such as ionic or covalent bonds.
31 Hydrophobic attachment of the agent may be particularly
32 required for certain embodiments, such as devices known
33 as "electronic noses" which detect the presence and/or
34 concentration of a gas. Preferably, the agent is
35 physically attached to the membrane, advantageously by
36 means of a covalent bond. It may be desirable for

1 certain agents to be attached to the membrane surface
2 via a spacer molecule so that presentation of the agent
3 is enhanced and/or that steric interference is reduced
4 or avoided.

5
6 Optionally more than one agent may be located on the
7 same filter and these agents may act independently of
8 each other on different substrates or may compete for
9 the same substrate. Optionally two or more agents may
10 sequentially modify the same original substrate. Thus
11 the first agent acts on the unmodified substrate,
12 producing an intermediate product. This intermediate
13 product is then modified or detected by a second agent.
14 A similar chain of reactions may be produced with any
15 number of different agents.

16
17 For certain applications the agent may be located on
18 the walls of the chamber which collects the filtrate,
19 or may be presented on beads, rods or the like located
20 within the chamber collecting the filtrate. Likewise
21 it is also possible for the agent to be similarly
22 located on the filtrant (unfiltered) side of the
23 membrane.

24
25 It is possible for different fluids to be present on
26 either side of the membrane, at least one of the fluids
27 being subject to (positive or negative) pressure so
28 that cross-filtration occurs. At least one component
29 of one fluid is thus caused to move across the membrane
30 and undergoes a chemical reaction with a component of
31 the other fluid. The presence and/or amount of product
32 may optionally be detected by a sensor.

33
34 An example of this embodiment is the treatment of
35 effluent containing at least one environmentally
36 unacceptable component, which may be rendered harmless

1 via chemical reaction or which is to be measured. The
2 required reactant is included in the fluid on the
3 opposite membrane side. Either the reactant moves
4 across the filter or, more preferably, the
5 environmentally unacceptable component moves across the
6 filter. The component may then either be subjected to
7 a chemical reaction following which the end product
8 thereof may either be discharged or collected
9 separately or, if desired, recycled. Alternatively the
10 component may be detected.

11

12 The filtration device may use positive or negative
13 pressure to control the ingress or egress of filtration
14 fluid and/or the rate of filtration. The pressure may
15 be reversible to allow "cleaning" of the membrane,
16 extending their working life.

17

18 Optionally the material to be sampled contains
19 particulate matter such as cell debris or cells. In
20 this situation the use of controlling pressure may be
21 particularly useful. Where cells are present it may be
22 desirable for the device to be a sealed unit so that
23 the filtration process is totally contained within the
24 filter cell.

25

26 In one preferred embodiment the volume between one
27 surface of a membrane and its boundary is at least
28 partially filled with a material. The material may be
29 either porous or non-porous depending on the intended
30 use of the device and the membrane selected for use.
31 Optionally, the volume defined between the membrane and
32 the outer casing may be substantially filled with the
33 material. Alternatively the material may fill separate
34 portions of that volume, thus sub-dividing it into
35 smaller discrete volumes. Suitable materials include
36 polymers (for example polymeric adhesives), especially

1 light curable or UV curable polymers. Specific mention
2 may be made of light or UV curable polymers available
3 from Ablestick Ltd (for example LCM 32, LCM 34 and LCM
4 35), Bostick Ltd or Dynax Inc (especially 191M) as
5 being useful in this regard. Non-porous materials
6 include solids through which parts of the filtrate can
7 diffuse, for example gels (such as agar gels) or the
8 like. The material may be introduced in liquid or
9 semi-liquid form and solidified in situ. The presence
10 of the porous material may enhance the speed of the
11 response times in testing for the presence and/or
12 amount of a test substance. The material may be chosen
13 having regard to fluid in the filter cell and any test
14 required.

15
16 As an example of this embodiment, a single hollow
17 membrane fibre, or a bundle of such fibres, may be
18 placed into an outer casing. The volume between the
19 inner surface of the casing and the outer surface of
20 the membrane fibre(s) may be filled with the material.
21 The material may be inserted into that volume by
22 injection and/or by capillary action. If required, the
23 material may be cured, for example by exposure to blue
24 light or to UV light. The mother liquor may then be
25 fed down the material-filled volume, with the challenge
26 or test substance being provided via the lumen of the
27 membrane, or vice versa.

28
29 Alternatively, if a membrane in the form of a sheet is
30 utilised, the material may fill at least part of the
31 volume between a membrane surface and its boundary,
32 normally the inner wall of the casing or a further
33 membrane sheet.

34
35 Where a material is present in the manner described
36 above, it is possible for the agent to be attached to,

1 contained within or encapsulated by the material.

2

3 In addition to a component-modifying agent located on
4 the filter, the device of the present invention may
5 optionally further comprise one or more detecting
6 agents or sensors. The sensor(s) may, for example,
7 monitor the level of modified component and optionally
8 also the level of modified component. In a preferred
9 embodiment the sensors are visually apparent or are
10 arranged to give a visual display of their output (for
11 example through a microprocessor or the like). Any
12 commercially available sensor may be used in the
13 apparatus of the present invention. Preferred examples
14 include light-emitting, photo-reactive or
15 photosensitive sensors.

16

17 Where the outer casing (and if present the material) is
18 optically suitable, it will be possible to use
19 colorimetric analysis to determine whether the test
20 substance is present and/or the amount thereof.
21 Desirably the presence of the test substance will be
22 due to a colour change and it may be preferable in
23 certain circumstances for the outer casing and/or
24 material to be optically clear.

25

26 A component-modifying agent may be, for example, an
27 enzyme, antibody, abzyme, a microbe (such as a bacteria
28 or virus), genetic material (such as DNA or RNA),
29 lectin, or any chemical reagent or catalyst, or any
30 combination or functional part thereof. Generally
31 where the agent is a biomolecule it will be attached
32 covalently to the filter via a spacer unit, for example
33 a carbon chain, optionally containing reactive groups,
34 eg acrylic acid or acrylamide or the like. In this
35 situation the agent is advantageously provided with any
36 co-factor or co-enzyme necessary for modification of

1 the component in the liquid to be processed. The co-
2 enzyme and/or co-factor may either be provided on the
3 surface of the filter or may be included in the liquid
4 being processed.

5

6 In a preferred embodiment the component of the liquid
7 to be modified is a sugar and the agent is a sugar
8 modifying enzyme, for example a saccharase.

9

10 Where the agent is a sugar modifying enzyme, preferably
11 a sugar degrading enzyme (for example a saccharase),
12 the device of the present invention is adapted to
13 process sugar containing liquids, so that the sugar
14 content of the processed liquid is altered, preferably
15 is substantially reduced.

16

17 In one particular embodiment the component is a sugar.
18 For example the component may be sucrose and the
19 modifying agent may be sucrase and thus cause
20 degradation of the sucrose into fructose and glucose.

21

22 In a further aspect, the present invention provides a
23 process of detecting or modifying a component of a
24 liquid substrate, wherein:

25

26 a. said liquid substrate is filtered by cross-flow
27 filtration through a device as described above,
28 the component being present in the filtrate; and

29

30 b. the filtered component is detected or modified by
31 an agent located on a filter in said device.

32

33 Alternatively the agent may be located on the filtrate
34 side of said filter.

35

36 Optionally said modified component is returned to the

1 filtrant of the liquid.

2

3 The membrane for use in the device of the invention may
4 be of any convenient shape and mention may be made of
5 hollow membrane fibres and flat sheet or tubular
6 membranes. Hollow membrane fibres or bundles of such
7 fibres may be preferred in certain situations since
8 this form permits a relatively large surface area
9 through which filtration may occur. For other
10 applications, however, flat membrane sheets (or bundles
11 of such sheets) may be preferable. The membranes may
12 contain pores of sizes from 0.001 to 30 microns in
13 diameter or alternatively may possess Molecular Weight
14 cut-off values from, for example 100 to 1,000,000 (eg
15 300 to 100,000, 500 to 1,000) Daltons.

16

17 The membrane may be made of any convenient material and
18 the present invention is not limited to the membrane to
19 be used. Generally the membrane will be selected for
20 the filtration size. Ceramic filters, for example, may
21 filter particles of diameter 5.0 μm to 0.1 μm and
22 hollow fibre membranes may filter molecules of 1 mDa to
23 5 kDa in suitable membranes are available commercially
24 and may be made of polysulphone, cellulose, cellulose
25 diacetate, polypropylene, ceramics materials and/or
26 other co-polymers.

27

28 The filtrate chamber may incorporate a sensor or
29 plurality of sensors that produce electrical signals in
30 response to changes in the chemical composition of the
31 filtrate or of the fluid surrounding the sensor, and
32 which sensors may be biosensors. Alternatively the
33 device may comprise an agent able to modify one of the
34 components of the fluid as described above.

35

36 The device may be adapted (optionally via a connector)

1 to form a close fit with syringe needles or syringe
2 bodies. This arrangement may be particularly
3 convenient where the sample to be tested is a
4 biological fluid (eg blood, synovial fluid or the
5 like). The syringe needle may itself be inserted into
6 the device, for example where the membrane is a single
7 hollow fibre the syringe needle may be inserted into
8 the lumen of the hollow fibre. Alternatively the
9 needle may be removed from the syringe and the neck of
10 the syringe connected into the device. The syringe
11 plunger may then be depressed, the fluid in the syringe
12 being expelled into the device and undergoing cross-
13 flow filtration followed by modification and/or
14 detection. Thus, an extremely quick and simple test
15 can be performed to give an "on-the-spot" diagnosis.

16
17 The device may be connected with pumps and tubing to
18 form an apparatus arranged so that mother liquor may be
19 continuously pumped through the device for separation
20 and sampling; and in which apparatus there may be
21 provision for returning the process liquor and/or
22 filtrate to the mother liquor.

23
24 The flow through the membrane may be directionally
25 reversible so that gel polarisation and/or cell
26 attachment may be eliminated or substantially
27 eliminated thus increasing the control and growth of
28 cells and the operational life of the process system.
29 Alternatively the flow rate may be reversed to increase
30 the rate of reaction occurring at the membrane.

31
32 The device of the invention may have no vents to the
33 atmosphere and may provide total containment for the
34 fluids in process. The system may be constructed of
35 materials that permit sterilisation of the system.

36

1 The device may in some embodiments have no vents to the
2 atmosphere and provides total containment for the
3 fluids being processed. The device may be constructed
4 of materials that permit sterilisation of the system.

5

6 To ensure hydrophilicity of membranes, consisting of
7 hydrophobic materials such as polypropylene, poly
8 carbonate and hydrophobic polysulphone, one should
9 follow the following general guidelines:

10

11 1. Use a solvent which wets the membrane and is
12 soluble in water. Usually this is done by using
13 96% ethanol solution.

14

15 2. Fill up the module (ie the interior of the
16 capillaries) with ethanol and keep them filled for
17 at least 10 minutes.

18

19 3. Replace the alcohol by water and apply reasonable
20 transmembrane pressure (max. 1.0 Bar) to force the
21 alcohol followed by water across the membrane.
22 Maintain this condition for about 10 minutes. For
23 a module with a membrane surface area of 1.0 m²
24 one will require a minimum of 2 litres of water.
25 Measure the flow rate of water.

26

27 4. After performing the above steps the membrane
28 should be ready for use.

29

30 In order to be able to use the hollow fibre membrane
31 filters over a longer period of time one should follow
32 the general cleaning procedure as outlined below:

33

34 1. After each filtration process rinse the hollow
35 fibre membrane filter thoroughly with distilled
36 water followed by an appropriate cleaning

- 1 solution: eg Decon-Neutracon Solution (neutral pH)
2 for general cleaning of filters used for proteins
3 and fatty substances. Rinse thoroughly afterwards
4 with distilled water.
5
- 6 2. The procedure should be followed by a rinsing
7 procedure in water.
8
- 9 3. The ceramic filters can be brushed after use to
10 clean the surface of the filter, followed by a
11 rinse procedure with appropriate cleaning
12 solutions and distilled water.
13
- 14 4. The hollow fibre membrane cartridges should be
15 sterilised when applicable with the appropriate
16 technique.
17
- 18 5. The membranes should be kept wetted after use. In
19 order to prevent the fibres from drying out, a 10-
20 20% alcohol solution should be used for this
21 purpose.
22
- 23 One should follow the general guidelines for
24 sterilising filters and other parts of the fluidlines
25 that are in contact with the fluids which are to be
26 processed. Details are to be found in the product
27 guidelines for eg autoclaves and steam sterilisers
28 supplied by various manufacturers. For those filters
29 that will not withstand the higher temperatures as used
30 for heat sterilising various chemical methods are
31 available to sterilise the filters in a safe and
32 efficient way.
33
- 34 1. NaOH solution 4% (60 minutes). Not for use with
35 cellulose or cellulose di-acetate filters.
36

1 2. Sterilising fluids for medical dialysing units
2 such as Dialina and Renalin Acetoper.

3
4 3. Peractic acid 3%.

5
6 4. Formalin 4%.

7
8 5. Ethylene Oxide (up to 800mg/l).

9
10 In one embodiment of the present invention there is
11 provided a device having a filter cell of low internal
12 volume and provided with an inlet tube carrying the
13 mother liquor (ie. the liquid before processing) from a
14 process vessel. The mother liquor in the inlet tube
15 may, if desired, be raised to a sufficient pressure to
16 cause filtrate to pass through a membrane in the cell
17 into a filtrate chamber of minimal volume and from
18 which chamber an outlet tube may be provided for
19 returning the filtrate to the process vessel. The
20 filtrate in the outlet tube may, if desired, be reduced
21 in pressure by suction to produce the pressure
22 differential required for filtration. The cell should
23 additionally have a second outlet tube on the mother
24 liquor side of the membrane so that the unfiltered
25 residue of the mother liquor may be returned directly
26 to the process vessel. The filtrate chamber may carry
27 in close proximity to the membrane a sensor or an array
28 of several sensors as well as a sampling port for the
29 removal of samples for external analysis. Preferably
30 the sensors may be bio-sensors, optical devices, pH
31 probes, conductivity electrodes or any other devices
32 for analysing the contents of the filtrate. The
33 membranes may be of any of the known ceramic or
34 polymeric micro- or ultra-filtration types in hollow
35 fibre or flat membranes forms.

36

1 In one embodiment the device is a processing and
2 handling system for liquids which controls, or removes
3 suspended or dissolved particles and substances in a
4 process liquor by filtration of the liquor through
5 micro- or ultra-filtration membranes and which system
6 may incorporate a direct sensor or plurality of sensors
7 so that specific soluble substances can be analysed
8 without interference with or contamination of the
9 sensors. In the system, control of the process can be
10 made rapidly by microprocessor or computer via a feed-
11 back loop system.

12

13 Thus the present invention provides a device for use as
14 a liquid handling system, the device allowing a
15 selective sample from a mother liquor to be taken,
16 which sample is free or substantially free from
17 substances of above or below a chosen particle or
18 molecular size. Desirably the device totally contains
19 all the fluids and materials being processed. The
20 device comprises a flow-through cell containing a
21 micro- or ultra-filtration membrane or a plurality of
22 such membranes arranged for separating ingredients of
23 differing particle or molecular size, and a filtrate
24 chamber in which the filtrate collects.

25

26 The flow-through cell may have provision for ingress of
27 unfiltered liquor at higher positive or negative
28 pressure.

29

30 In another embodiment, a separating and sampling device
31 for fluids is provided which is capable of taking a
32 selective sample from a mother liquor, which sample is
33 free or substantially free from substances of above a
34 chosen particle or molecular size. The device
35 comprises a flow-through cell containing a micro- or
36 ultra-filtration membrane or a plurality of such

1 membranes arranged for cross-flow filtration. The
2 device has a filtrate chamber in which the filtrate
3 collects for examination. The cell has provision for
4 ingress of unfiltered liquor at higher pressure and
5 egress of filtered liquor at lower pressure. The
6 membrane or membranes may be in the form of a sheet, of
7 tube or of hollow fibres and may contain pores of sizes
8 from 0.001 to 30 microns in diameter. The membranes
9 may possess Molecular Weight cut-off values from 300 to
10 1,000,000 Daltons. The filtrate chamber may
11 incorporate a sensor or plurality of sensors that
12 produce electrical signals in response to changes in
13 the chemical composition of the fluid surrounding the
14 sensor. The sensors may be biosensors. Optionally the
15 device may be incorporated along with pumps and tubing
16 into an apparatus arranged so that mother liquor may be
17 continuously pumped through the device for separation
18 and sampling. In such an apparatus there may be
19 provision for returning the filtered liquor and/or
20 filtrate to the mother liquor; and also the flow
21 through the membrane may be reversed in direction so
22 that gel polarisation may be eliminated or
23 substantially eliminated thus increasing the working
24 life of the cell.

25
26 By way of example embodiments of the invention and uses
27 therefor are shown in Figures 1-11.

28
29 Figures 1 to 5 schematically illustrate various
30 embodiments of the device according to the invention;

31
32 Figure 6 is a perspective view of one embodiment of a
33 device according to the invention, with a cut-away
34 section to illustrate the membrane fibres;

35
36 Figure 7 is a schematic diagram of a process circuit in

1 which the device according to the present invention can
2 be used;

3

4 Figures 8 and 9 are further schematic diagrams
5 illustrating a device according to the present
6 invention.

7

8 Figures 10 and 11 illustrate two embodiments adapted to
9 support cell growth and, optionally cellular challenge.

10

11 In more detail, Figure 1 shows the device indicated
12 generally at 1 having a flat sheet membrane filter 2
13 which separates the flow-through cell 3 from the
14 filtrate chamber 4. Process liquor is pumped at
15 pressure through the cell in the direction shown by the
16 arrow and the filtrate may leave the filtrate chamber 4
17 by a port 5 which may be fitted with a tap (not shown).
18 Alternatively a further fluid may be input via port 5
19 and be filtered across membrane 2. An agent may be
20 located on the membrane filter 2, cell 3 and/or in
21 chamber 4.

22

23 Figure 2 illustrates a device similar to that shown in
24 Figure 1 and described above. In the device of Figure
25 2 (shown generally at 1) the filter membrane 2 is in
26 the form of a tube 6. The mother liquor is passed
27 through the lumen of tube 6 (which forms flow-through
28 cell 3), preferably at a controlled pressure, in the
29 direction of the arrow. The filtrate will collect in
30 chamber 4 and may be taken off via port 5 which again
31 may if desired be fitted with a tap. Alternatively
32 port 5 may be used to input a second fluid, either to
33 react with the filtrate of the mother liquor (ie the
34 agent may be present in the second fluid) or to control
35 the pressure within the device.

36

1 Figure 3 illustrates a further embodiment, similar to
2 those previously described with respect to Figures 1
3 and 2. In the embodiment of Figure 3 the membrane
4 filter (shown generally at 2) is in the form of hollow
5 fibre membranes 7 of which two are illustrated for
6 simplicity. The number of hollow fibre membranes may
7 be adjusted from 1 to several hundred depending upon
8 the size of the device. The lumen of the individual
9 fibres are used to transport the mother liquor into the
10 device and thus act as the flow-through cell. The
11 filtrate collects in chamber 4. The ends of the hollow
12 fibres are sealed into the device to prevent the mother
13 liquor entering the filtrate chamber 4 by any means
14 other than by passing across the membrane.

15
16 Figure 4 depicts a further embodiment of device 1 with
17 tubular filter membrane 2 as depicted in Figure 2 but
18 with the addition of a direct sensor 8. The sensor 8
19 may be, for example, a pH sensor, a conductivity sensor
20 or a biosensor. In use the component of interest
21 passes across the membrane filter 2 into the filtrate
22 chamber 4. The pressure differential across the
23 membrane may be controlled via port 5 which may contain
24 a tap or valve. The component of interest may react
25 with or otherwise be detected by sensor 8 which then
26 generates production of an output signal, preferably an
27 electrical, audible or visual output signal.

28
29 Figure 5 illustrate three further embodiments of a
30 device according to the present invention. In general
31 the embodiments shown are similar to those described
32 above for Figures 1 to 4, especially Figure 3. In
33 Figure 5A, the membrane 2 consists of a single hollow
34 fibre membrane, having an internal lumen of
35 approximately 1mm. The whole of the volume between the
36 exterior surface of the membrane and the interior

1 surface of the outer casing 9 is filled with a material
2 11, such as LCM 32 or LCM 35 from Ablestick, which
3 contains an agent able to react with a component of
4 interest in the mother liquor. In use the mother
5 liquor is passed down the lumen of the hollow fibre
6 membrane 7 and filtrate moves across the membrane
7 surface by cross-flow filtration. The component of
8 interest present in the filtrate then encounters the
9 agent held within the material 11. In the illustrated
10 embodiment the material is solid and the agent is
11 uniformly distributed therein. However a porous
12 material encapsulating the agent could equally be used.
13 The component may either be modified by reacting with
14 the agent or may be simply detected by the agent which
15 may not alter it physically or chemically. For example
16 the agent could be light emitting, photosensitive or
17 photoreactive.

18
19 In Figure 5B the material 11 does not entirely fill the
20 volume between the exterior surface of the membrane and
21 the interior surface of the outer casing 9, but leaves
22 a pre-determined volume able to accept filtrate. The
23 agent may be present either in the free volume or else
24 be held within material 11 as described for Figure 5A
25 above. Alternatively two different agents may be
26 present in these separate physical locations.

27
28 Although not illustrated, the device of Figure 5B could
29 also be produced having two or more (for example three,
30 four or five) volumes separately filled with material
31 11 (or with different types of material 11) and
32 separated or abutting each other. Again different
33 agents or different concentrations of agents could be
34 contained in each.

35

36 In Figure 5C, the device is as shown in Figure 5B,

1 except that the device further includes a additional
2 port 5. Port 5 may be used to draw off filtrate, to
3 introduce a second fluid, optionally containing an
4 agent to modify or detect the component of interest or
5 simply to adjust the pressure and thus the flow across
6 the membrane.

7
8 In Figure 6, device 1 is fitted with a membrane filter
9 2 which separates the flow-through cell 3 from the
10 filtrate chamber 4. Process liquor is pumped by pump
11 17 at positive or negative pressure through the device
12 1 in the direction shown by the arrow. The filtrate
13 leaves the filtrate chamber 4 by a port 5 and is sensed
14 by a direct sensor 8, for example a pH sensor, a
15 conductivity sensor or a biosensor. Excess unfiltered
16 fluid exits via port 10. In the device illustrated
17 part of the outer casing is absent in order to
18 illustrate the membrane filter 2 used which is shown to
19 consist of multiple hollow fibres 7 as in Figure 3.
20 However other forms of membrane filters 2 can also be
21 used.

22
23 Figure 7 shows a process vessel 12 in which cells are
24 being cultured under agitation using stirrer 30 and in
25 which the glucose concentration requires to be
26 continuously monitored. A peristaltic pump 17 pumps
27 the mother liquor from the vessel to an inlet port 13
28 in a device 1 according to the present invention. The
29 device illustrated is that shown in Figure 6, but any
30 of the other embodiments could likewise be used. Pump
31 17 maintains sufficient pressure to cause filtration
32 through a hollow fibre membrane filter 2. Within the
33 filter cell is a glucose bio-sensor 8 which measures
34 the quantity of glucose in the filtrate and the
35 filtrate may be returned to the process vessel through
36 outlet tube 14 and the residual unfiltered liquor may

1 be returned to the process vessel through outlet tube
2 15.

3
4 Figure 8 shows the filter cell incorporated in a
5 working system in which the process liquor is passed by
6 a pump 17 through a pressure sensor 20 to the device
7 according to the invention 1, fitted with a direct
8 sensor 8 which is monitored by a direct sensor assay
9 instrument 16. The process liquor exits from the
10 device 1 through a second pressure sensor 20a and a
11 second pump 17a which is adjusted in pumping rate
12 relative to the pumping speed of the first pump 17 to
13 control the pressure in the device 1. Filtrate
14 accumulates in the filtrate chamber 4 (not shown) and
15 is pumped from it by the third pump 17b by way of a
16 third pressure sensor 20b. The process liquor is
17 returned to the process via connecting tubes (not
18 shown) and the filtrate is directed through a multi-
19 port valve 18 to an external analytical system 19 for
20 further analysis, or to a drain or filtrate store 21,
21 or to a filtrate return line 22 in which it may join
22 the sampled process liquor returning to the process.

23
24 Figure 9 shows the device 1 according to the invention
25 incorporated in a working system in which the process
26 liquor is passed by a pump 17 through a pressure sensor
27 20 to the filter cell 1, fitted with a direct sensor 8
28 which is monitored by a direct sensor assay instrument
29 16 which can be microprocessor or computer controlled.
30 The process liquor exits from the device 1 through a
31 second pressure sensor 20a and a second pump 17a which
32 is adjusted in pumping rate relative to the pumping
33 rate of the first pump 17 to control the pressure in
34 the device 1. Filtrate accumulates in the filtrate
35 chamber 4 (not shown) and is pumped from it by the
36 third pump 17b by way of a third pressure sensor 20b.

1 Within the enclosed circuit of pumps 17, 17a and 17b
2 and pressure sensors 20, 20a and 20b processing of
3 material within the device 1 can be achieved at above
4 and below atmospheric pressure on both sides of the
5 membrane 2 (not shown). The process liquor is returned
6 to the process and the filtrate is directed through a
7 multi-port valve or valves 18 to an external analytical
8 system 19 for further analysis, or to drain or filtrate
9 store 21 or to a filtrate return line 22 in which it
10 may join the sampled process liquor returning to the
11 process. If the process involves cell culture, at the
12 end of the process, mature cells or cells ready for
13 harvest can be flushed out of the circuit and collected
14 via line to container 23. This can be achieved
15 continuously or in discreet batches. The whole system
16 is constructed of materials that can be sterilised.

17
18 An additional sampling circuit is illustrated whereby a
19 sample can be withdrawn to testing unit 24 and can
20 either be held in test 25 or returned via pump 17c to
21 the process circuit. Testing unit 24 may be an
22 additional sensor and assay instrument. Alternatively
23 unit 24 may be used to incorporate a substance to the
24 process liquor.

25
26 2Figure 10 shows a device according to the invention
27 shown generally at 1, the membrane filter lumen being
28 shown in dotted lines. In the embodiment shown pump 17
29 pushes cell growth medium around a closed loop made up
30 of line 26 and device 1. Present in line 26 is an
31 outlet means (generally a tap or valve) 27, a sensor 8
32 and also injection or withdrawal means (here
33 illustrated as syringes, but the invention is not so
34 limited) 28a and 28b. The injection or withdrawal
35 means 28a and 28b may be used either to introduce
36 factors exhausted from the medium due to cell growth or

1 may take a sample of the medium from the closed loop
2 for analysis. This latter option may be of interest
3 where the cells grown on the medium are producing a
4 factor or substance which is of interest.

5
6 Multiple devices 1 according to the invention may be
7 incorporated into a single closed loop arrangement as
8 is shown in Figure 11. The system may be under the
9 control of microprocessor or computer 35. Multiple
10 injection or withdrawal means 28 (illustrated as
11 syringes) are selectively connectible to individual
12 devices 1 by valves 29 in lines 26. The devices can be
13 connected to biosensors 8 and a line 32 including a
14 pressure sensor 33 and a displacement pump 34 can be
15 used to adjust pressure in the circuit. Collection
16 bays 31 can be provided at various locations for
17 collection of filtrate or mother liquor from specific
18 device, as required. The precise layout of any
19 particular system can be different from that
20 illustrated.
21

1 CLAIMS

2

3 1. A device to process a fluid, the device having a
4 membrane filter, wherein an agent able to detect
5 or cause modification of at least one component of
6 said fluid is localised in said device.

7

8 2. A device according to Claim 1 wherein said agent
9 is localised on said membrane filter.

10

11 3. A device according to either one of Claims 1 and 2
12 wherein filtration of the fluid occurs by cross-
13 filtration.

14

15 4. A device according to any one of Claims 1 to 3
16 wherein the device further comprises a sensor.

17

18 5. A device according to any one of Claims 1 to 4
19 wherein the membrane filter is a single hollow
20 fibre or multiple hollow fibres.

21

22 6. A device according to Claim 5 wherein the membrane
23 filter is a single hollow fibre.

24

25 7. A device according to any one of Claims 1 to 6
26 wherein the volume between one surface of a
27 membrane and its boundary is at least partially
28 filled with a porous substance.

29

30 8. A device according to Claim 7 wherein the porous
31 substance contains said agent.

32

33 9. A device according to any one of Claims 1 to 8
34 wherein the agent is an enzyme, antibody, abzyme,
35 a microbe, genetic material, lectin, a chemical
36 reagent, a catalyst, or a function part or any

1 combination thereof.

2

3 10. A process of detecting or modifying a component of
4 a liquid substrate, wherein:

5

6 a. said liquid substrate is filtered by cross-
7 flow filtration through a device as claimed
8 in any one of Claims 1 to 9, the component
9 being present in the filtrate; and

10

11 b. the filtered component is detected or
12 modified by an agent located on a filter in
13 said device.

14

15 11. A process as claimed in Claim 10 wherein the agent
16 is a cell culture and said component is a nutrient
17 required for cell growth.

18

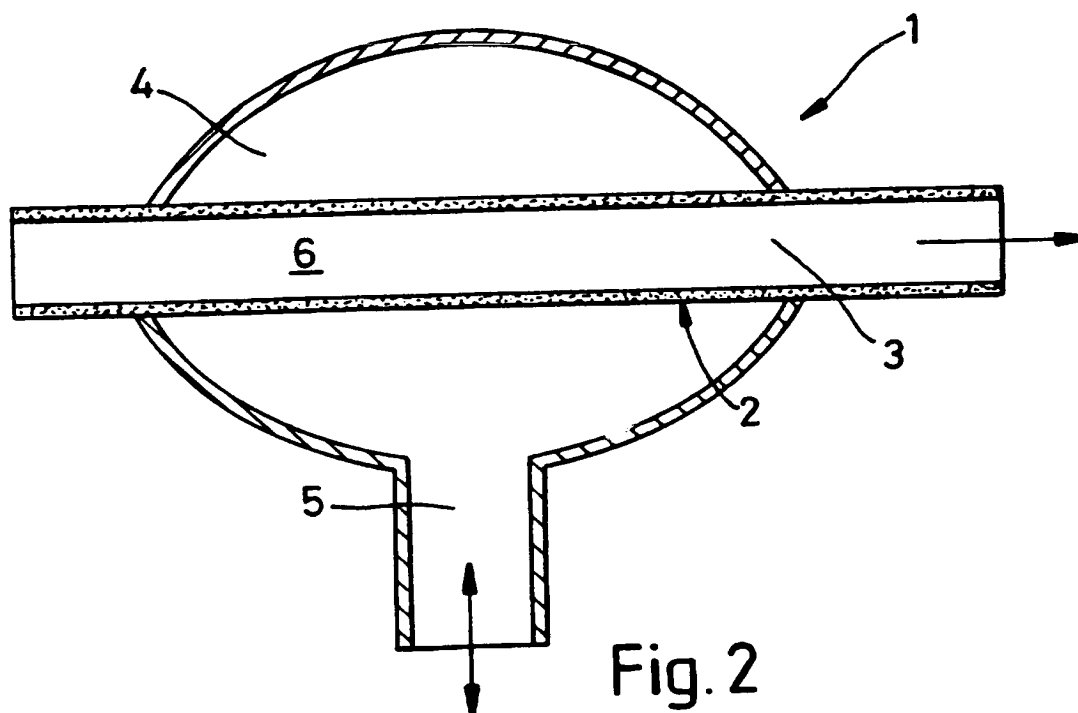
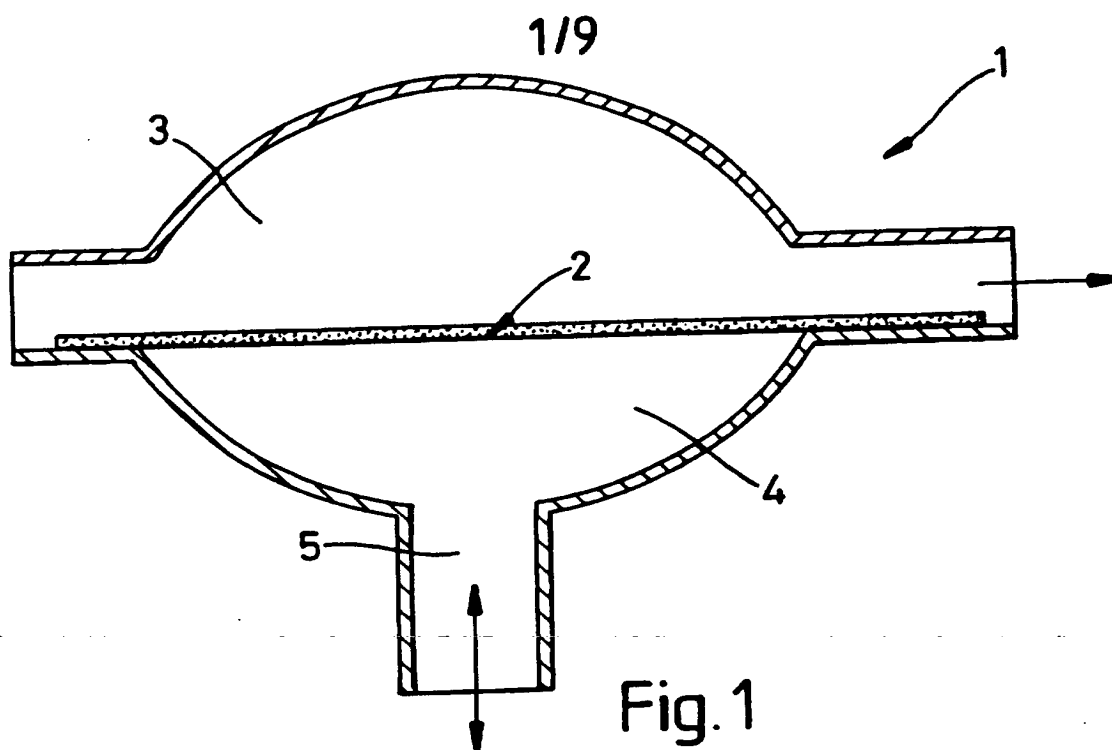
19 12. A process as claimed in Claim 10 wherein the
20 liquid substrate is a waste product and said agent
21 detects or renders harmless an undesirable
22 component of said waste product.

23

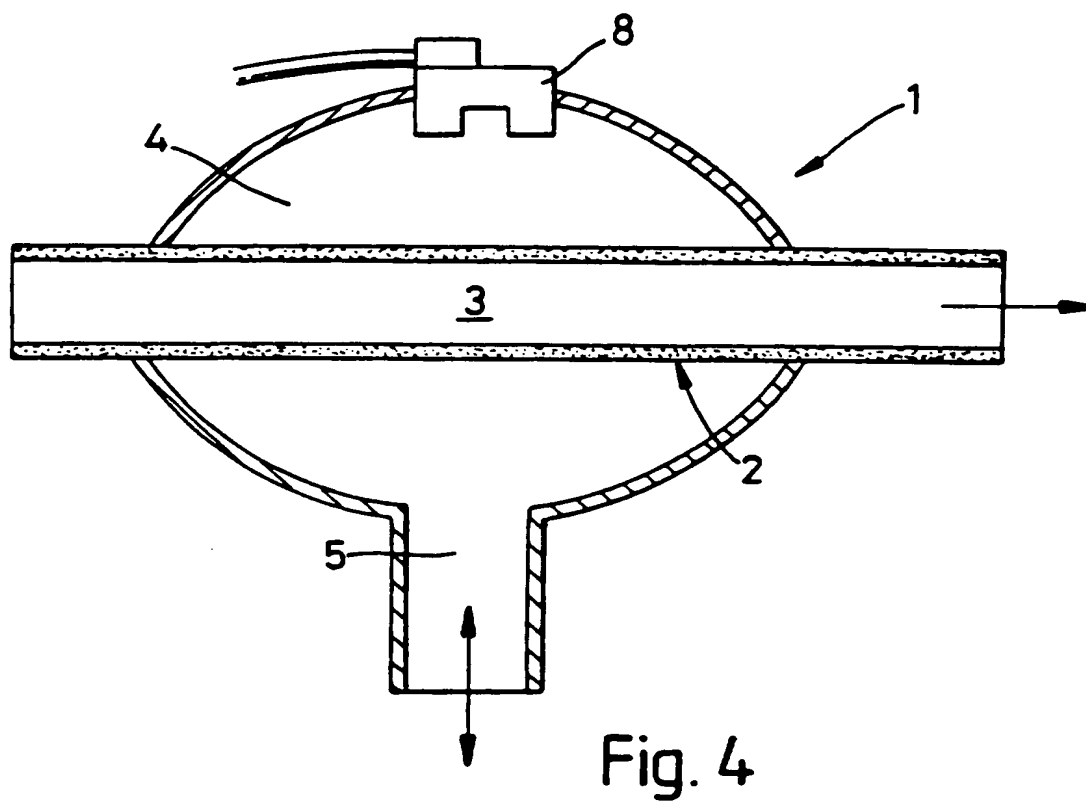
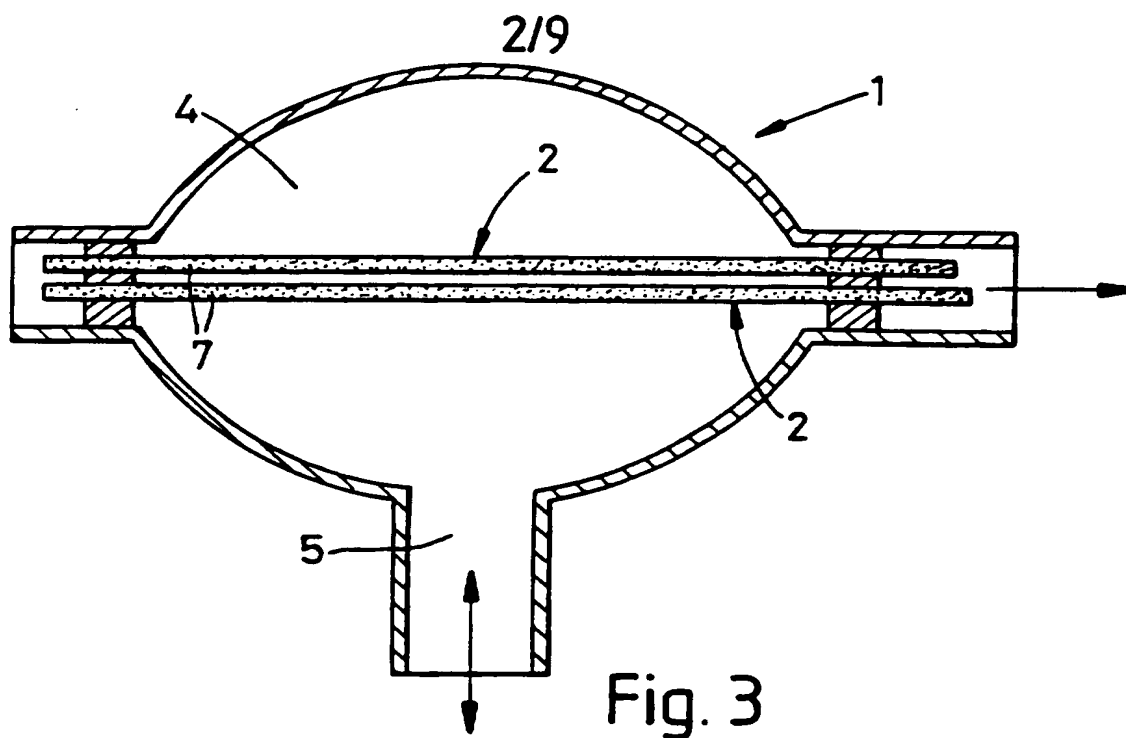
24 13. A process as claimed in Claim 10 wherein the
25 liquid substrate is or comprises a biological
26 sample and said agent detects a component of said
27 sample.

28

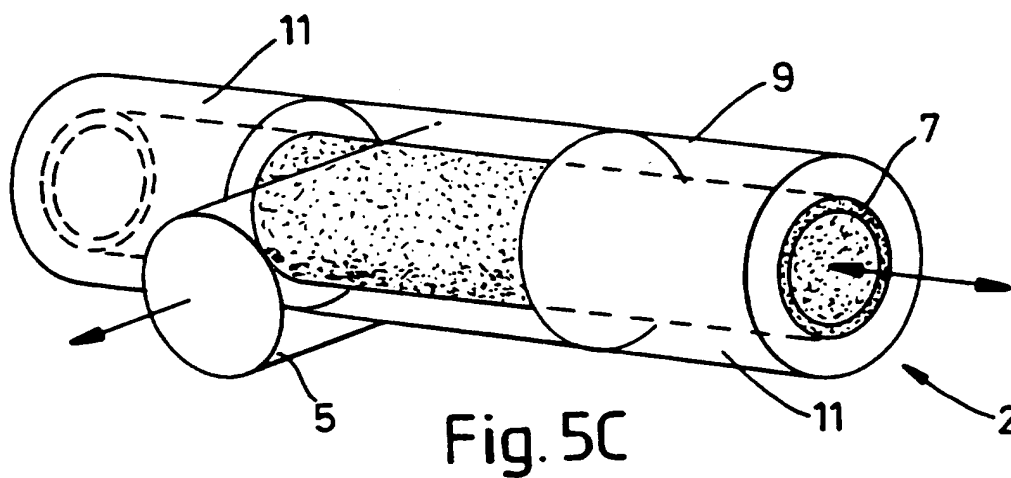
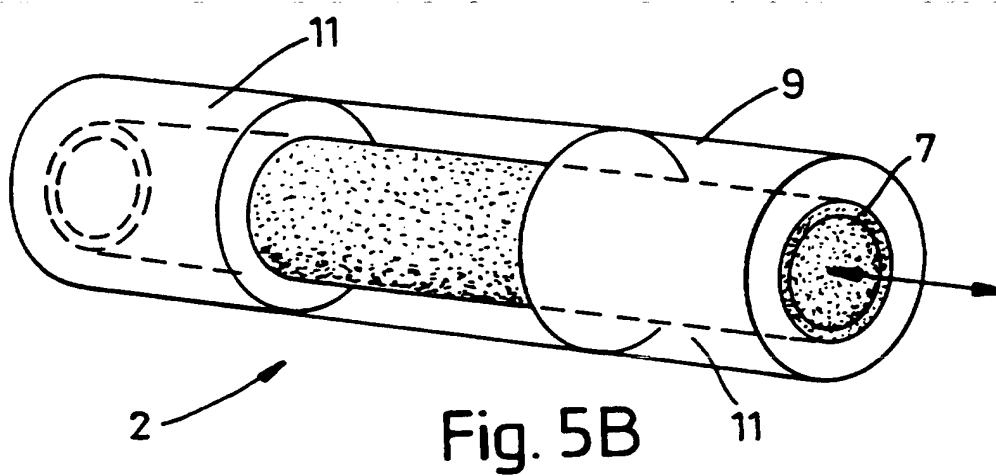
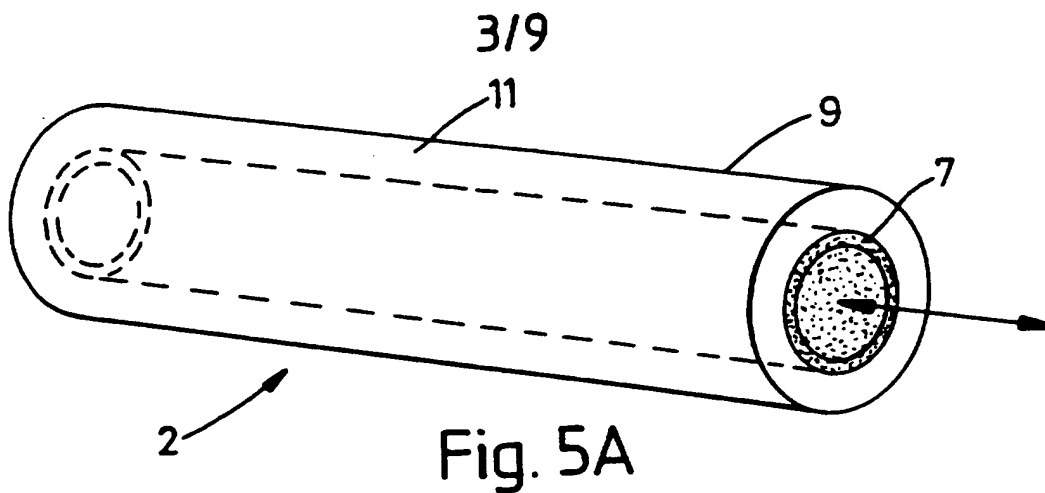
29 14. A method of diagnosis, said method comprising
30 subjecting a test liquid comprising a biological
31 sample from a patient to a process as claimed in
32 Claim 10, wherein said agent is able to
33 selectively detect the presence and/or amount of
34 component within said liquid.



SUBSTITUTE SHEET (RULE 26)



SUBSTITUTE SHEET (RULE 26)



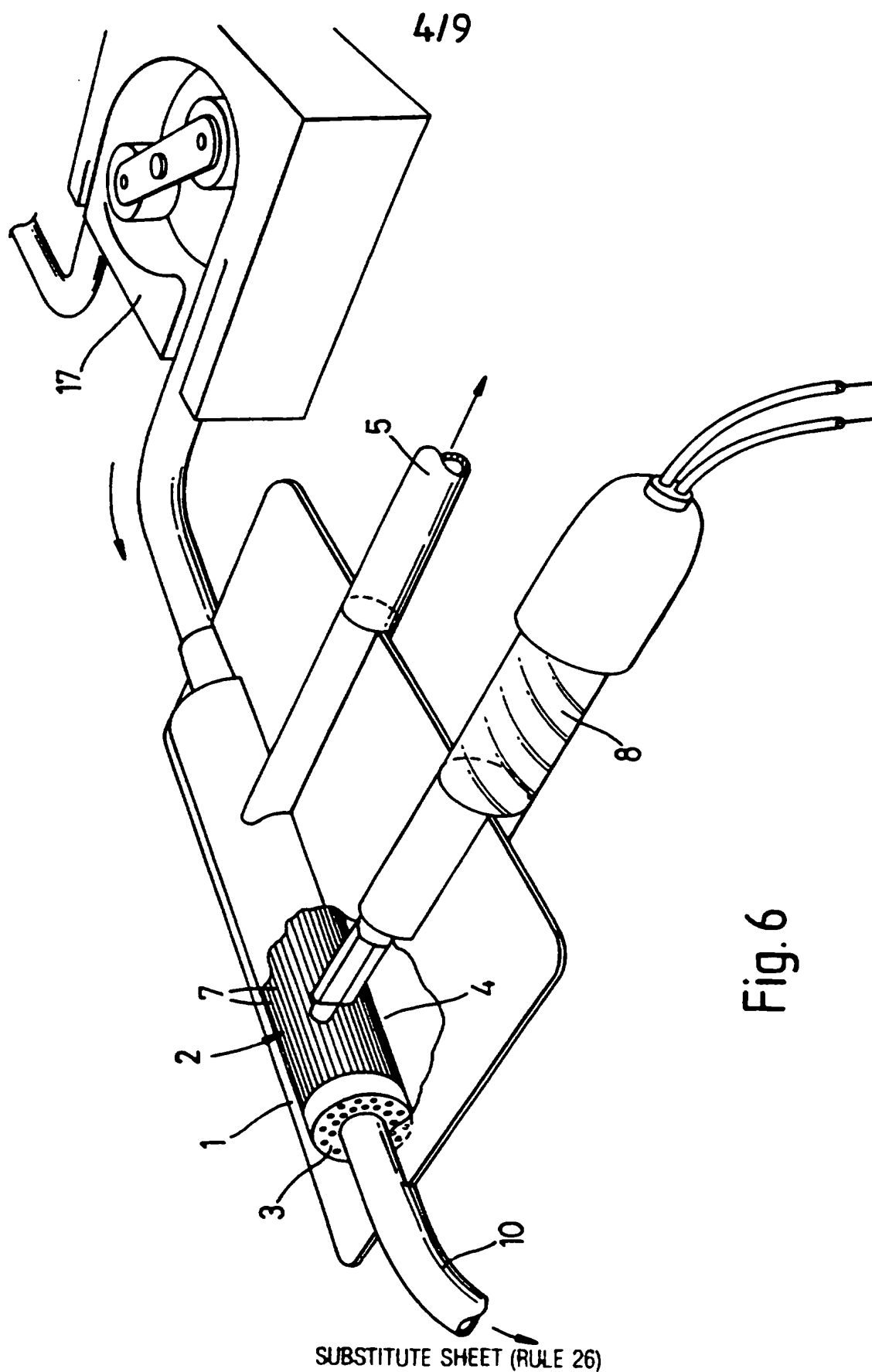


Fig. 6

SUBSTITUTE SHEET (RULE 26)

5/9

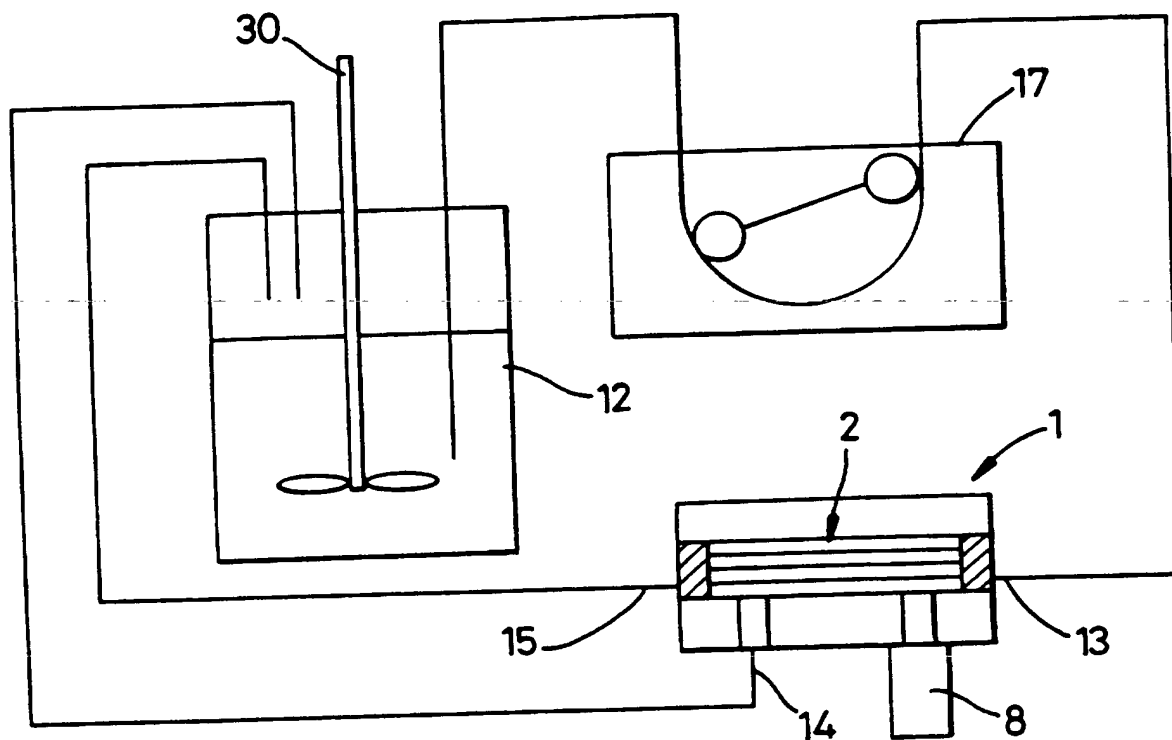


Fig. 7

6/9

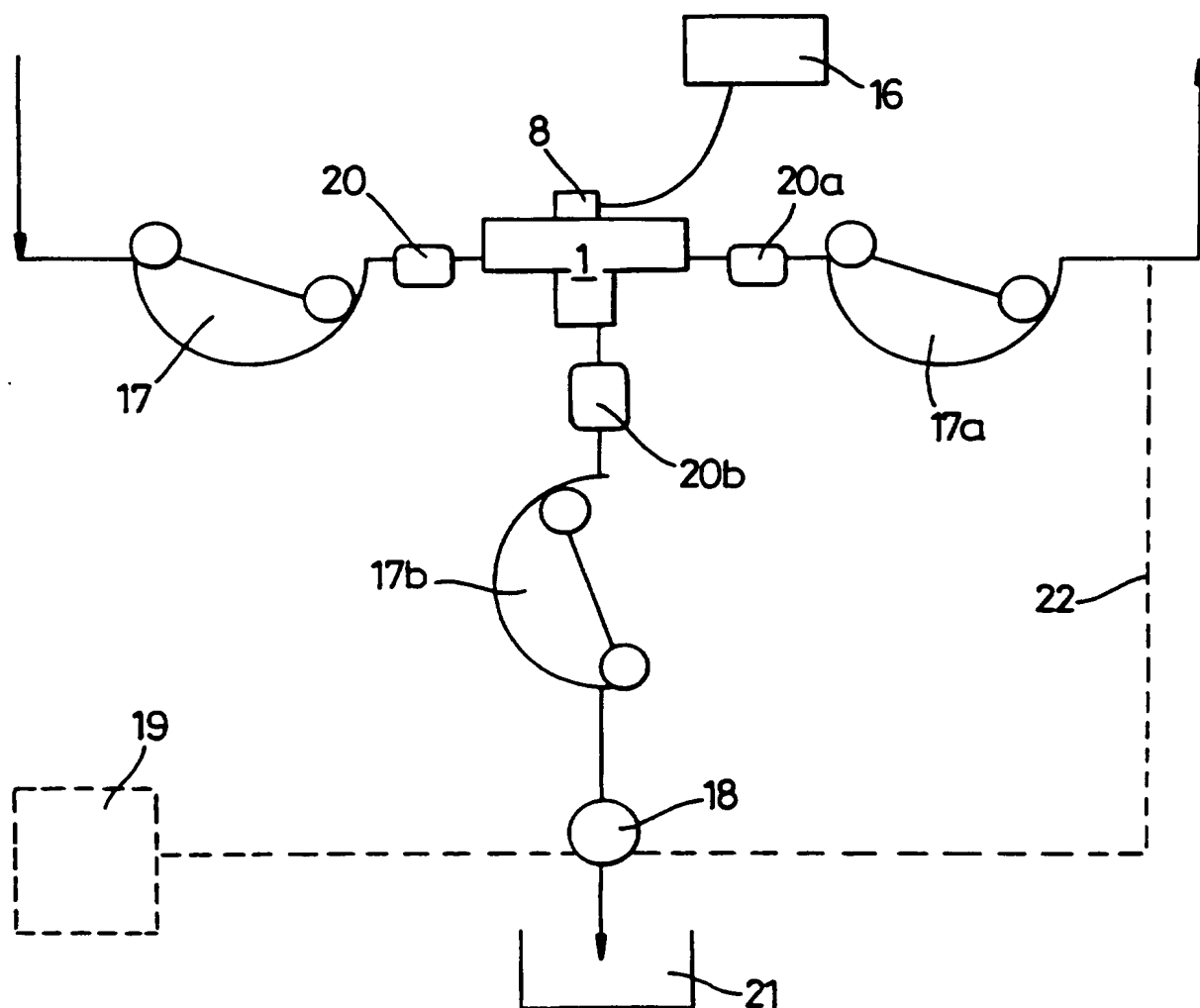


Fig. 8

7 / 9

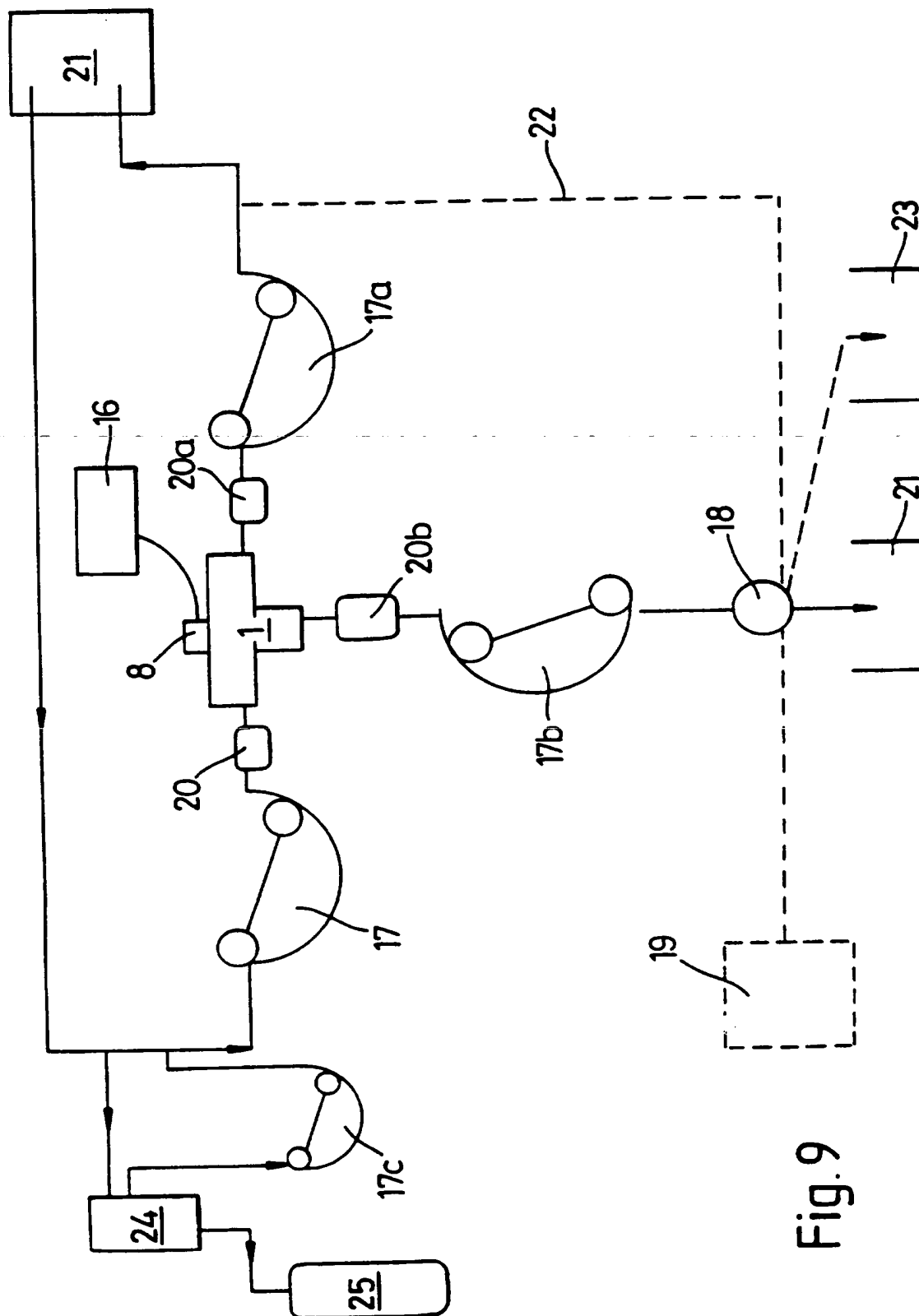


Fig. 9

SUBSTITUTE SHEET (RULE 26)

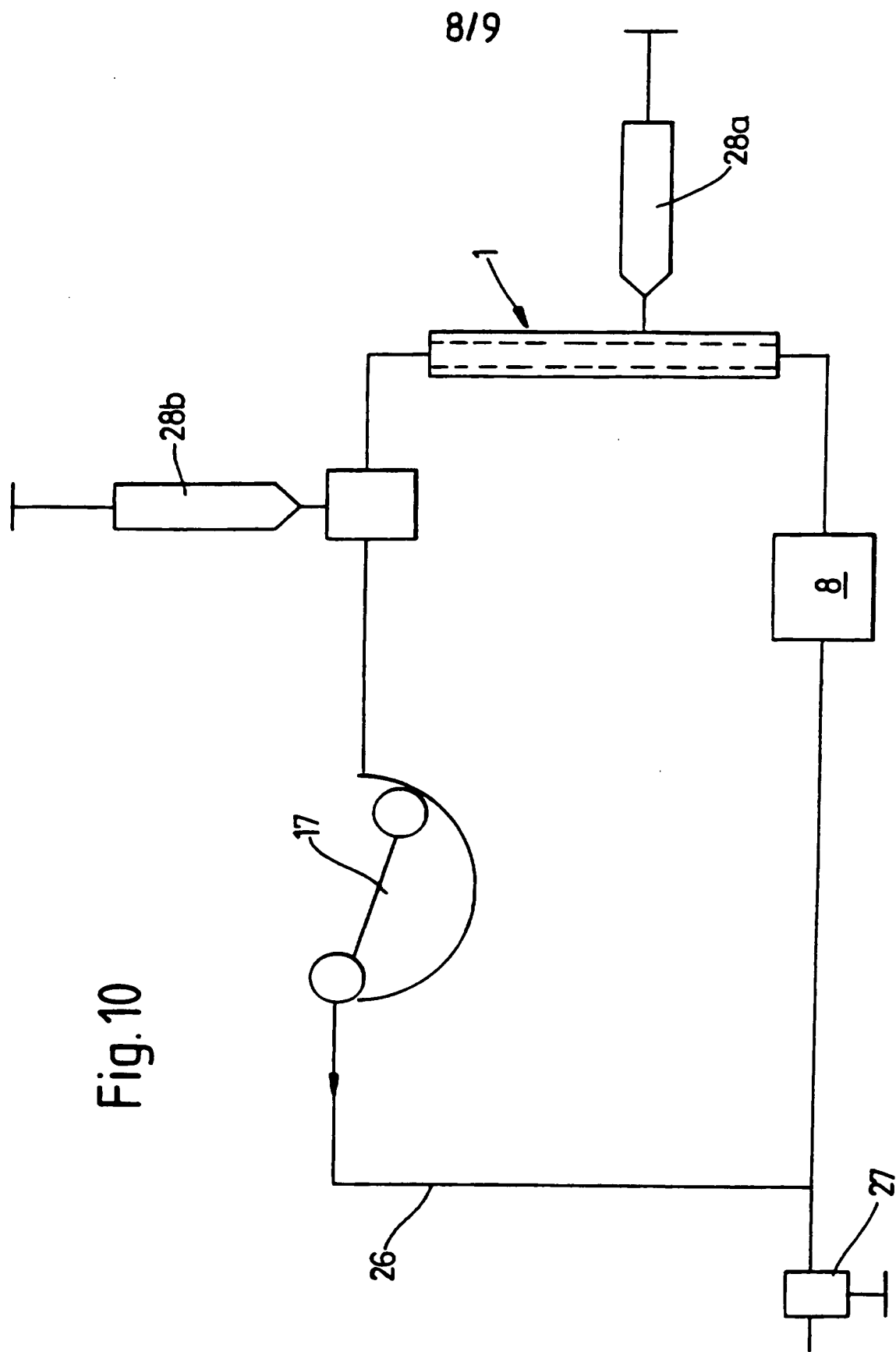


Fig. 10

SUBSTITUTE SHEET (RULE 26)

9 / 9

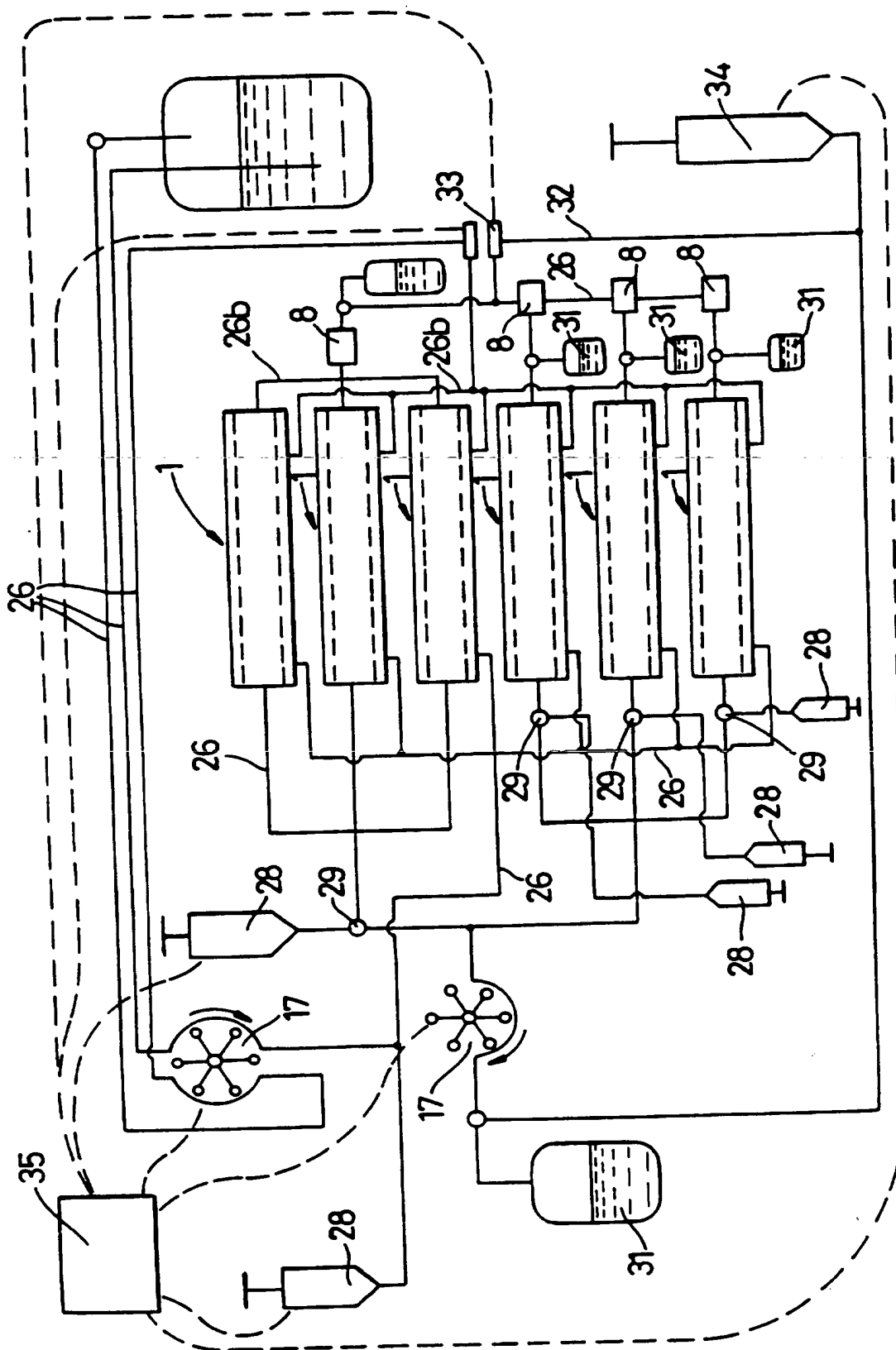


Fig.11

SUBSTITUTE SHEET (RULE 26)

INTERNATIONAL SEARCH REPORT

International Application No
PCT/GB 95/01834

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 B01D61/00 G01N33/48

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 6 B01D

Documentation searched other than minimum: documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US,A,4 685 463 (R. B. WILLIAMS) 11 August 1987 see the whole document ---	1,3-6,9, 10,13,14
X	US,A,4 311 789 (U. T. G. NYLEN ET AL.) 19 January 1982 see the whole document ---	1,3-10, 13,14
X	FR,A,2 640 643 (L'OREAL) 22 June 1990 see the whole document ---	1-4,9, 10,13,14
X	WO,A,93 06045 (IMPERIAL COLLEGE OF SCIENCE, TECHNOLOGY & MEDICINE) 1 April 1993 see the whole document ---	1-3,9, 10,12
-/--		

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents:

- * A* document defining the general state of the art which is not considered to be of particular relevance
- * E* earlier document but published on or after the international filing date
- * L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- * O* document referring to an oral disclosure, use, exhibition or other means
- * P* document published prior to the international filing date but later than the priority date claimed

* T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

* X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

* Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

* &* document member of the same patent family

Date of the actual completion of the international search

28 November 1995

Date of mailing of the international search report

01-12-1995

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+ 31-70) 340-2040, Tx. 31 651 epo nl,
Fax (+ 31-70) 340-3016

Authorized officer

Devisme, F

INTERNATIONAL SEARCH REPORT

International Application No
PCT/GB 95/01834

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP,A,0 120 285 (NIPPON OIL AND FATS CO, LTD) 3 October 1984 see the whole document ---	1,3,5,9, 10
X	WO,A,87 02381 (SEPRACOR, INC.) 23 April 1987 see the whole document ---	1,3,5-10
X	EP,A,0 541 245 (EXXON RESEARCH AND ENGINEERING CO) 12 May 1993 see the whole document ---	1-3,9,10
X	EP,A,0 228 885 (NGK INSULATORS, LTD.) 15 July 1987 see the whole document ---	1,3,9,10
X	EP,A,0 155 237 (MBR BIO REACTOR AG) 18 September 1985 see the whole document ---	1,3,4, 7-11
P,X	WO,A,94 16800 (TYGOLA PTY. LTD.) 4 August 1994 see the whole document ---	1,9
A	GB,A,2 252 260 (MEDICAL RESEARCH INTERNATIONAL) 5 August 1992 see the whole document -----	1,7

INTERNATIONAL SEARCH REPORT

Information on patent family members

National Application No

PCT/GB 95/01834

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
US-A-4685463	11-08-87	NONE	
US-A-4311789	19-01-82	SE-B- 396819 AT-B- 361131 AU-B- 504818 AU-B- 2101176 BE-A- 850006 CA-A- 1075136 CH-A- 631546 DE-A- 2658101 FR-A, B 2337341 GB-A- 1581353 JP-A- 52085885 NL-A- 7614448 SE-A- 7600024 US-A- 4229542	03-10-77 25-02-81 01-11-79 06-07-78 15-04-77 08-04-80 13-08-82 14-07-77 29-07-77 10-12-80 16-07-77 04-07-77 02-07-77 21-10-80
FR-A-2640643	22-06-90	CA-A- 2005624 DE-T- 68907197 EP-A, B 0384090 JP-A- 3103224 US-A- 5250419	16-06-90 20-01-94 29-08-90 30-04-91 05-10-93
WO-A-9306045	01-04-93	AU-A- 2588592 CA-A- 2119383 EP-A- 0604514 JP-T- 6510696	27-04-93 01-04-93 06-07-94 01-12-94
EP-A-120285	03-10-84	JP-C- 1844457 JP-A- 59154999 DE-A- 3485748 US-A- 5024942	25-05-94 04-09-84 02-07-92 18-06-91
WO-A-8702381	23-04-87	US-A- 4795704 AU-B- 597284 AU-B- 6473986 CA-A- 1289493 DE-A- 3688908 DE-T- 3688908 EP-A, B 0243404	03-01-89 31-05-90 05-05-87 24-09-91 23-09-93 20-01-94 04-11-87

INTERNATIONAL SEARCH REPORT

Information on patent family members

national Application No

PCT/GB 95/01834

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO-A-8702381		JP-T- 63501612 KR-B- 9405577 SU-A- 1787044	23-06-88 21-06-94 07-01-93
EP-A-541245	12-05-93	US-A- 5210059 CA-A- 2078973 JP-A- 5237395	11-05-93 11-04-93 17-09-93
EP-A-228885	15-07-87	JP-C- 1766147 JP-B- 4051211 JP-A- 62160121 DE-D- 3650155 DE-T- 3650155 US-A- 4865630	11-06-93 18-08-92 16-07-87 12-01-95 06-04-95 12-09-89
EP-A-155237	18-09-85	DE-A- 3409501 JP-A- 60210982	24-10-85 23-10-85
WO-A-9416800	04-08-94	AU-B- 5966394	15-08-94
GB-A-2252260	05-08-92	NONE	